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AM0065 / Version 02 Sectoral Scope: 04, 09 and 11 EB 41

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# Approved baseline and monitoring methodology AM0065

"Replacement of SF<sub>6</sub> with alternate cover gas in the magnesium industry"

# I. SOURCE, DEFINITIONS AND APPLICABILITY

#### Sources

This baseline and monitoring methodology is based on the following proposed new methodologies:

- NM0212 "SF<sub>6</sub> Switch at Dead Sea Magnesium" prepared by EcoTraders;
- NM0222 "Conversion of SF<sub>6</sub> to the Alternative Cover Gas SO<sub>2</sub> in Magnesium Production in China" prepared by QualityTonnes.

This methodology also refers to the latest approved version of the following tool:

• Combined tool to identify the baseline scenario and demonstrate additionality.

For more information regarding the proposed new methodology and the tool as well as its consideration by the Executive Board please refer to <<u>http://cdm.unfccc.int/goto/MPappmeth</u>>.

#### Selected approach from paragraph 48 of the CDM modalities and procedures

"Existing actual or historical emissions, as applicable"

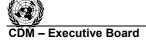
## Definitions

For the purpose of this methodology, the following definitions apply:

The **magnesium metal casting industry**, for the purposes of this methodology, is defined as being included in one or more of the following industry segments:

- Primary ingot casting (includes alloying furnaces, does not refer to primary magnesium production from metallic magnesium such as electrolysis or thermal reduction processes);
- Die casting;
- Gravity casting;
- Production of secondary magnesium through recycling of magnesium or its alloys;
- A cover gas is an inert gas used to avoid oxidation of molten magnesium in casting and alloying processes.





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# Advanced "dilute SO<sub>2</sub>" melt protection technology is technology that meets the following specifications:

- Well controlled SO<sub>2</sub> concentration and flow rates with concentration typically one percent or less. An associated <u>SO<sub>2</sub> exhausting and abatement system</u> to ensure SO<sub>2</sub> emissions are in compliance with the local environmental regulations. Emissions from the facility to the ambient air should comply with the local standards of the country. If no local standards exist, the following value should be taken into account as a cap limit for SO<sub>2</sub> concentration in the exhausting system – 1470 mg/m<sup>3</sup> (dry basis, 273 K, 101,325 kPa at an oxygen concentration of 6 %(v/v);
- Precise gas mixing and delivery system using mass flow controllers (MFC) or similarly accurate device and heated gas lines to SO<sub>2</sub>;
- Gas cabinet or cylinder storage area with leak monitors and emergency ventilation system.
- Redundant / back-up melt protection technology in case SO<sub>2</sub> leak requires system shut-down and repair;
- Emergency response plan, training, and personal safety equipment;
- Back-up power / generator for gas mixing system and necessary controls, compressors, etc. capable of running independently for 12 hours;
- Maintenance plan for equipment and gas distribution system to assure safe and consistent operation.

# Applicability

This methodology applies to project activities that replace the use of cover gas  $SF_6$  in full or in part by another cover gas, HFC134a, Perfluoro-2-methyl-3-pentanone ( $CF_3CF_2C(O)CF(CF_3)_2$ ) or  $SO_2$  using lean  $SO_2$  technology, <u>in existing facilities</u><sup>1</sup>.

The methodology is applicable under the following conditions:

- All segments of the magnesium industry (as defined in Definitions section above) where SF<sub>6</sub> is replaced;
- If SO<sub>2</sub> is used as cover gas in the project activity, only "dilute SO<sub>2</sub>" technology is used which meets the definition provided in the Definitions section above;
- Local regulations in the host country regarding SO<sub>2</sub> emissions in the exhausting system should be complied with. If such regulations are not in place, the following value should be taken into account as a cap limit of SO<sub>2</sub> concentration in the exhausting system 1470 mg/m<sup>3</sup> (dry basis, 273 K, 101,325 kPa at an oxygen concentration of 6 %(v/v).

The methodology is only applicable if the baseline scenario is the continuation of current practice of using  $SF_6$  as a cover gas.

<sup>&</sup>lt;sup>1</sup> The facility has an operating history of at least three years prior to validation.



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The methodology is <u>not</u> applicable to the following:

- Sectors other than magnesium that use SF<sub>6</sub>; or
- Project activities that replace the use of SF<sub>6</sub> with salt fluxes, or sulfur powder;
- New facilities.

In addition, the applicability conditions included in the tool referred to above apply.

## **II. BASELINE METHODOLOGY PROCEDURE**

#### Identification of the baseline scenario

Project participants shall apply the procedures detailed in the latest version of the "Combined tool to identify the baseline scenario and demonstrate additionality" to identify the baseline scenario.

When applying the "Combined tool to identify the baseline scenario and demonstrate additionality", the following guidance should be taken into account:

## Step 1: Define alternative scenarios to the proposed CDM project activity

In the magnesium sector these alternatives may include the use of:<sup>2</sup>

- (a) Advanced "dilute SO<sub>2</sub>" melt protection technology;
- (b) SF<sub>6</sub>- continuation of current practice;
- (c) HFC134a;
- (d) Perfluoro-2-methyl-3-pentanone;
- (e) SF<sub>6</sub> capture and reuse;
- (f) Process modifications / optimizations to minimize SF<sub>6</sub> consumption.

## Step 2: Barrier analysis

The main barriers relevant to this sector are technological barriers and barriers due to prevailing practice. <u>Technological Barriers</u>

The use of advanced "dilute  $SO_2$ " melt protection technology (scenario 1), HFC 134a (scenario 3), Perfluoro-2-methyl-3-pentanone (scenario 4) for melt protection is an entirely new technique that is being introduced to the magnesium sector due to the sectors growing awareness concerning climate change.

<sup>&</sup>lt;sup>2</sup> As realistic and credible scenarios should be identified in cases where  $SF_6$  is currently being used, it would be unrealistic and not credible to assume that projects that have advanced to the superior cover gas technology of using  $SF_6$  shall regress technologically to using salt fluxes, sulfur powder, or  $SO_2$  (old technology). Despite the facts that these technologies have been implemented previously, these technologies are still considered a technological regression in the case  $SF_6$  is being currently used.



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### Step 3: Investment Analysis

If investment analysis is undertaken, then each scenario should include in the financial indicator a calculation of all relevant costs. These should include, if relevant (but are not limited to):

- Cost of retrofitting equipment to work on alternate cover gas;
- Cost of installing new equipment to work on alternate cover gas;
- Additional maintenance and training costs due to the SF<sub>6</sub> switch;
- Cost of raw material;
- Cost of new safety measures (in the case of advanced "dilute SO<sub>2</sub>" melt protection technology), including the abatement system;
- Payment of royalty fees.

The financial analysis should also consider the actual quantity of cover gas used. For example the quantity of HFC134a needed is 50% in comparison to SF<sub>6</sub>.

It should be noted that an ex-ante estimation of project emissions and the quantity of cover gas used in the project scenario may be required to conduct a financial analysis for the additionality assessment. In this case project emissions can be calculated by estimating the amount of alternative cover gas used and multiplying it by the calculated GWP weighting of the estimated by-products. The GWP weightings are based on defaults and do not change during the crediting period. To calculate ex-ante project emissions, one only needs to know how much cover gas is likely to be used. The ratio of cover gas to  $SF_6$  may not be 1:1. In other words, it is possible that less or more cover gas may be required to provide the same level of protection as  $SF_6$ . In these cases, it is assumed that tests would be carried out on the alternative gas before the project is implemented. These tests would provide the plant managers with the amount of gas that would be needed to provide the desired level of protection. This number, along with the GWP weightings and the estimated magnesium production over the crediting period, should provide a reasonable estimate of project emissions. The sensitivity analysis should include financial calculations based on variations on this assumption.

#### Additionality

The additionality of the project activity shall be demonstrated and assessed using the latest version of the "Combined tool to identify the baseline scenario and demonstrate additionality".

#### **Project boundary**

The **spatial extent** of the project boundary encompasses the specific industrial process in the magnesium plant where  $SF_6$  was used as a cover gas and is being replaced with the alternate cover gas. The greenhouse gases included in or excluded from the project boundary are shown in Table 1.



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	Source	Gas	Included ?	Justification / Explanation
Baseline	Cover gas mix to protect	CO <sub>2</sub>	No	Used in some cases as diluent to $SF_6$ in the cover gas mix. Since it is used both in baseline and project scenarios, for the sake of simplicity it is excluded from both calculations. When $CO_2$ is used only in the baseline activity, it will not be included as a conservative assumption.
Bas	molten	SF <sub>6</sub>	Yes	Major source of emissions in the baseline.
	magnesium	CH <sub>4</sub>	No	$CH_4$ is excluded from the baseline calculations. Exclusion of this gas is conservative.
		N <sub>2</sub> O	No	N <sub>2</sub> O is excluded from the baseline calculations. Exclusion of this gas is conservative.
Project activity	Inserted as cover gas mix to protect molten magnesium	CO <sub>2</sub>	Yes/No	Used as diluent in the cover gas mix. If it is used both in baseline and project scenarios, it is excluded from both calculations. If used only in project scenario, it is included in project emissions calculations.
		HFC- 134a, Perflu oro-2- methyl -3- pentan one	Yes	Replacement gas to $SF_6$ . Must be considered in project emission calculations. This source will be taken into account if the cover gas used is HFC-134a or Perfluoro-2-methyl-3-pentanone.
		$SF_6$	Yes	In cases where SF <sub>6</sub> is used in the project scenario, it is included in project emission calculations and monitored data.
	By-product of reaction between cover gas mix and molten magnesium	CH <sub>4</sub>	Yes	Accounted for through the calculation of project emissions. This source will be taken into account if the cover gas used is HFC-134a or Perfluoro-2-methyl-3- pentanone.
		N <sub>2</sub> O	Yes	Accounted for through the calculation of project emissions. This source will be taken into account if the cover gas used is HFC-134a.
		C <sub>2</sub> F <sub>6</sub>	Yes	Accounted for through the calculation of project emissions. This source will be taken into account if the cover gas used is HFC-134a or Perfluoro-2-methyl-3- pentanone.
		C <sub>3</sub> F <sub>8</sub>	Yes	Accounted for through the calculation of project emissions. This source will be taken into account if the cover gas used is Perfluoro-2-methyl-3-pentanone.

# Table 1: Emissions sources included in or excluded from the project boundary

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(2)

#### **Baseline emissions**

<u>Case-1</u>: In case historical annual consumption for  $SF_6$  and magnesium production per equipment k in each segment j is available, baseline emissions shall be calculated using the following equations:

$$BE_{y} = \sum_{j} \sum_{k} (EF_{SF6,Mg,k,j} * P_{Mg,PJ,k,j,y}) * GWP_{SF6}$$
(1)

Where:

$BE_{y}$	= Baseline emissions in year y (tCO <sub>2</sub> e/yr)
EF <sub>SF6,Mg,k,j</sub>	= Baseline emission factor for each equipment k in each segment j.( $tSF_6/tMg$ )
P <sub>Mg,PJ,k,j,y</sub>	= Annual amount of Mg products manufactured in project scenario in each equipment $k$
	in each segment <i>j</i> per year <i>y</i> .
GWP <sub>SF6</sub>	= Global Warming Potential of $SF_6(tCO_2e/tSF_6)$

For each equipment *k* in each segment *j* and year *y*:

$$EF_{SF6,Mg,k,j} = Min\{\frac{C_{SF6,EM,BL,k,j}}{P_{Mg,BL,k,j}}\}$$

y = 1,2,3 (each of corresponding to the last three years before the implementation of the project activity)

Where:

P <sub>Mg,BL,k,,j,y</sub>	= Annual Amount of Mg products manufactured in baseline scenario in each equipment
	k of each segment j (tMg/yr) for each year y of the three years prior to the project.
	One year data may be used in case 3 years data are not available (tMg/ yr). Amount of
	Mg products manufactured in baseline scenario in each equipment <i>k</i> of each segment <i>j</i>
	(tMg/ yr). Minimum of the last three years prior to validation (1 year data can be used)
	in case 3 years data are not available) should be used.
C <sub>SF6,EM,BL,k,j,y</sub>	= SF <sub>6</sub> actually emitted in the baseline in each equipment k of each segment j in year y.

 $C_{SF6,EM,BL,k,j,y} = SF_6$  actually emitted in the baseline in each equipment k of each segment j in year y. (tSF<sub>6</sub>/ yr)

$$C_{SF6,EM,BL,k,j,y} = C_{SF6,CON,BL,k,j,y} * DF_{SF6} * DI_{SF6,CON,BL,k,j}$$
(3)

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Where:	
C <sub>SF6,CON,BL,k,j</sub> ,y	= Annual consumption of SF <sub>6</sub> in the industrial facility in each equipment k of
	each segment <i>j</i> , in the baseline in year <i>y</i> calculated for each year <i>y</i> of the year/s prior to the project for the last three years (or one year if three-year data is not available)
	before the project's implementation. (tSF6/ yr).
	Total annual consumption of SF <sub>6</sub> in the industrial facility in each equipment <i>k</i> of
	each segment <i>j</i> , in the baseline. (tSF <sub>6</sub> / yr).
DF <sub>SF6</sub>	= Degradation Factor of SF <sub>6</sub> that reacts with the magnesium in the production process
	assumed as 0.5. <sup>3</sup>
DI <sub>SF6,CON,BL,k,j</sub>	= A conservative factor portraying the Data Integrity of $C_{SF6,CON,BL,j}$ in each equipment
	k of each segment j (Fraction), estimated as per information in Data and Parameters

For the purpose of ex ante baseline calculations for reporting in the CDM-PDD, future production levels shall be assumed as the past 3-year minimum production levels i.e.  $P_{Mg,PJ,k,j,y} = P_{Mg,BL,k,j}$ . The Annual Consumption of  $SF_6(C_{SF6,CON,BL,k,j})$  shall be estimated as the minimum of the following values:

- Minimum of Annual consumption of SF<sub>6</sub> in each equipment k of each segment j for the last three years prior to validation (1 year data can be used in case 3 years data are not available) (C<sub>SF6,EST,BL,k,j</sub>);
- Total consumption of SF<sub>6</sub> in each equipment k of each segment j, per year as per the 2006 IPCC Guidelines (C<sub>SF6,IPCC,BL,k,j</sub>):

$$C_{SF6,IPCC,BL,k,j} = C_{SF6,SPIPCC} * P_{Mg,BL,k,j}$$

not monitored section.

Where:

 $C_{\text{SF6},\text{SPIPCC}}$ 

Specific consumption of SF<sub>6</sub> in each equipment k of each segment j as per 2006 IPCC Guidelines (0.001t SF<sub>6</sub>/t Mg casting)

<u>**Case-2:**</u> In case <u>only</u> the historical annual consumption for  $SF_6$  for the <u>total</u> facility is available, baseline emissions shall be calculated using the following equations:

$$BE_{y} = P_{Mg,PJ,y} * GWP_{SF6} * EF_{SF6,Mg}$$

(5)

(4)

<sup>&</sup>lt;sup>3</sup> The Board after due consideration of available literature and structural design of the magnesium production facilities arrived at the conclusion that in absence of a proper system to collect the covers gases and exhaust, the uncertainties in current procedures to estimate the SF<sub>6</sub> destruction are very high. Therefore, a conservative default has been provided to ensure that emission reductions credited are real. Project Proponents are encouraged to submit to the DOE new procedures for undertaking measurement on project site to estimate the destruction efficiency. Procedures should be sufficiently robust, based as much as possible in International Standards and properly documented to ensure reliable estimates. The procedures should be based on experimentation of sufficient duration taking into account the variability in equipment used in different segments, variations in operating conditions/ practices, different type of alloys manufactured and similar other real-time production issues.

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Where: $BE_y$ $EF_{SF6,Mg,j}$ $P_{Mg,PJ,k,y}$ $GWP_{SF6}$	<ul> <li>Baseline emissions in year y (tCO<sub>2</sub>e/yr)</li> <li>Baseline emission factor for the facility calculated as the m 3 years of data (tSF<sub>6</sub>/ tMg)</li> <li>Annual amount of Mg products manufactured in project sc equipment k in each segment j per year y.</li> <li>Global Warming Potential of SF<sub>6</sub>(tCO<sub>2</sub>e/ tSF<sub>6</sub>)</li> </ul>	
$EF_{SF6,Mg} = M$	$\left\{ \frac{C_{SF6,EM,BL,y}}{P_{Mg,BL,Total,y}} \right\}$	<mark>(6)</mark>
y = 1,2,3 (corr	esponding to the last three years before the implementation of t	he project activity)
Where: P <sub>Mg,BL,TOTAL</sub> ,,y	<ul> <li>Total Amount of Mg products manufactured in baseline sc y for each year y-of the 3 years prior to the project. One ye data are not available (tMg/yr).</li> </ul>	
C <sub>SF6,EM,BL</sub> ,y	= Total SF <sub>6</sub> actually emitted in the baseline in the facility $\frac{1}{100}$	<mark>year y</mark> . (tSF <sub>6</sub> / yr)

 $C_{SF6,EM,BL} = C_{SF6,CON,BL} * DF_{SF6} * DI_{SF6,CON,BL}$ 

C <sub>SF6,CON,BL</sub>	= Total annual consumption of $SF_6$ in the industrial facility, in the baseline,( $tSF_6$ / yr).
DF <sub>SF6</sub>	= Degradation Factor of $SF_6$ that reacts with the magnesium in the production process
	assumed as 0.5. <sup>4</sup>
DI <sub>SF6,CON,BL</sub>	= A conservative factor portraying the Data Integrity of $C_{SF6,CON,BL}$ (Fraction),

estimated as per information in Data and Parameters not monitored section.

(7)

<sup>&</sup>lt;sup>4</sup> The Board after due consideration of available literature and structural design of the magnesium production facilities arrived at the conclusion that in absence of a proper system to collect the covers gases and exhaust, the uncertainties in current procedures to estimate the SF<sub>6</sub> destruction are very high. Therefore, a conservative default has been provided to ensure that emission reductions credited are real. Project Proponents are encouraged to submit to the Board request for revision of the methodology describing new procedures for undertaking measurement on project site to estimate the destruction efficiency. Procedures should be sufficiently robust, based as much as possible in International Standards and properly documented to ensure reliable estimates. The procedures should be based on experimentation of sufficient duration taking into account the variability in equipment used in different segments, variations in operating conditions/ practices, different type of alloys manufactured and similar other real-time production issues.



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For the purpose of ex ante baseline calculations for reporting in the CDM-PDD, future production levels shall be assumed as the past 3-year minimum production levels i.e.  $P_{Mg,PJ,jk,y} = P_{Mg,BI,TOTAL}$ . The Annual Consumption of SF<sub>6</sub> (C<sub>SF6,CON,BL</sub>) shall be estimated as the minimum of the following values:

- Minimum of Annual TOTAL consumption of SF6 in the facility for the last three years prior to validation (1 year data can be used in case 3 years data are not available) (CSF6,TOT,BL);
- Total consumption of SF6 in the facility, per year as per the 2006 IPCC Guidelines (CSF6,IPCC,BL) as per following equation:

$$C_{SF6,IPCC,BL} = C_{SF6,SPIPCC} * P_{Mg,BL,TOTAL}$$

(8)

# **Project emissions**

Project emissions include:

- Emissions from the cover gas used; HFC-134a or Perfluoro-2-methyl-3-pentanone;
- Emissions from the use of SF<sub>6</sub>, if any;
- Emissions from the consumption of CO<sub>2</sub> in case it is only used in the project scenario and not in the baseline.

Project emissions are calculated as follows:

$$PE_{y} = PE_{ALTGAS,y} + PE_{SF6,y} + \sum_{j,y} C_{CO2,PJ,j,y}$$
(9)

Where:

$PE_y$	= Project emissions in year $y$ (tCO <sub>2</sub> e/yr)
PE <sub>ALTGAS,y</sub>	= Project emissions from the use of HFC134a or Perfluoro-2-methyl-3-pentanone, if it is
	used as cover gas in project scenario - summing of all segments $j$ - in year $y$ (tCO <sub>2</sub> e/yr)
$PE_{SF6,y}$	= Project emissions from the use of SF <sub>6</sub> - summing of all segments $j$ - in year $y$
	(tCO2e/yr)
C <sub>CO2,PJ,j,y</sub>	= Consumption of $CO_2$ gas in project scenario for each segment per year. Shall be used
	when $CO_2$ is used as diluent in cover gas mix in the project scenario alone (i.e. not in
	the baseline scenario) (tCO2/yr)

Project emissions from the use of alternate gas

$$PE_{ALTGAS,y} = \sum_{j} \sum_{k} C_{ALTGAS,PJ,k,j,y} * GWP_{ALTGAS} * CF$$
(10)

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Where:

C <sub>ALTGAS,PJ,k,j,y</sub>	= Consumption of alternate gas in project scenario for each equipment k in each segment
	<i>j</i> per year (t / yr)
<b>GWP</b> <sub>ALTGAS</sub>	= Global Warming Potential of alternate gas. In case of using Perfluoro-2-methyl-3-
	pentanone the value used is 1
CF	= Conservative Factor. To compensate for the uncertainty in the global warming

potential of the by products emitted after the degradation of the alternate gas (default value of 1.26 for HFC134a and 2,830 for Perfluoro-2-methyl-3-pentanone<sup>5</sup>)

Project emissions from the use of SF<sub>6</sub>

$$PE_{SF6,y} = \sum_{j} \sum_{k} C_{SF6,EM,PJ,k,j,y} * GWP_{SF6}$$
(11)

Where:

C <sub>SF6,EM,PJ,k,,j</sub>	= $SF_6$ actually emitted in the project scenario in each equipment k of each segment j, per	•
	year y (tSF <sub>6</sub> / yr)	
GWP <sub>SF6</sub>	= Global Warming Potential of $SF_6$ (tCO <sub>2</sub> e/ tSF <sub>6</sub> )	

$$C_{SF6,EM,PJ,k,j,y} = C_{SF6,CON,PJ,k,j,y} * DF_{SF6,k,j} * DI_{SF6,CON,PJ,k,j,y}$$
(12)

Where:

C <sub>SF6,CON,PJ,k,j,y</sub>	= Total consumption of $SF_6$ in the project scenario in each equipment k for each segment
	j, per year y (tSF <sub>6</sub> / yr)
DF <sub>SF6,k,j</sub>	= Degradation Factor of $SF_6$ that reacts with the magnesium in the production process
	assumed as 0.5.
DI <sub>SF6,CON,PJ,k,j,y</sub>	= A conservative factor portraying the Data Integrity of $C_{SF6,CON,PJ,k,j,y}$ in each segment,
	per year. (Fraction), estimated as per information in Data and Parameters not
	monitored section.

Ex-Ante estimation of the consumption of HFC134a in the project scenario

 $C_{ALTGAS,PJ,j,y}$  shall be calculated ex-ante for the purpose of estimating emission reductions in the CDM-PDD with the following equation:

$$C_{ALTGAS, PJ, k, j, y} = C_{SF6, CON, BL, k, j} * 0.5$$
(13)

For the purpose of ex ante project emission calculations for reporting in the CDM-PDD, future production levels shall be assumed as the past 3 year maximum production level i.e.  $P_{Mg,PJ,k,j,y} = P_{Mg,BL,k,j}$ .

<sup>&</sup>lt;sup>5</sup> Based on the combination of the maximum values as per test results provided in EPA, "Characterization of Cover Gas Emissions from U.S. Magnesium Die Casting", Office of Air and Radiation, May 2004.





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When <u>only</u> the historical annual consumption for  $SF_6$  for the <u>total</u> facility is available:

$$\sum_{j} \sum_{k} C_{ALTGAS, PJ, k, j, y} = C_{SF6, CON, BL} * 0.5$$

# Ex-Ante estimation of the consumption of Perfluoro-2-methyl-3-pentanone in the project scenario

 $C_{ALTGAS,PJ,k,j,y}$  shall be calculated ex-ante for the purpose of estimating emission reductions in the CDM-PDD. If the cover gas used by the project activity is Perfluoro-2-methyl-3-pentanone, then  $C_{ALTGAS,PJ,j,y}$  will be estimated as the theoretical amount of Perfluoro-2-methyl-3-pentanone necessary for the future production , which can be estimated as the past 3 year maximum production levels i.e.  $P_{Mg,PJ,j,k,y} = P_{Mg,BL,k,j}$ .

## Leakage

No leakage is expected from the project activity.

#### **Emission reductions**

Emission reductions are calculated as follows:

$$ER_y = BE_y - PE_y$$

Where:

ERy	= Emission reductions in year $y$ (tCO <sub>2</sub> e/yr)
$BE_y$	= Baseline emissions in year $y$ (tCO <sub>2</sub> e/yr)
PE <sub>v</sub>	= Project emissions in year $y$ (tCO <sub>2</sub> /yr)





# Data and parameters not monitored

ID Number:	1
Data/Parameter:	GWP <sub>SF6</sub>
Data unit:	tCO2e/tSF6
Description:	Global Warming Potential of SF <sub>6</sub>
Source of data:	CDM EB
Measurement	Prior to the renewal of a crediting period it should be assessed if GWP values have
procedures (if any):	changed.
Any comment:	

ID Number:	2
Data/Parameter:	$P_{Mg,BL,k,i,y}$
Data unit:	tMg /yr
Description:	Amount of Mg products manufactured in baseline scenario in each equipment k of
	each segment j per year y of the last three years before the project's
	implementation (tMg/ yr).
Source of data:	Industrial Facility
Measurement	Measured by calibrated scales according to on-site working procedures
procedures (if any):	
Any comment:	Scales are usually calibrated frequently since this parameter is essential to the core
	business of the plant. Calibration frequency shall follow on-site calibration
	procedures.
	Minimum of the last three years prior to validation (1 year data can be used in case
	3 years data are not available) should be used.

ID Number:	3
Data/Parameter:	C <sub>SF6,EST,BL,k,j</sub>
Data unit:	tSF <sub>6</sub>
Description:	Mimimum of Annual consumption of $SF_6$ in each equipment k of each segment j
	for the last three years prior to validation (1 year data can be used in case 3 years
	data are not available)
Source of data:	Industrial Facility
Measurement	Measuring flow rates and integrating over time (flow measurement method)
procedures (if any):	
Any comment:	In case historical annual consumption for $SF_6$ per equipment k in each segment j is
	available





ID Number:	4
Data/Parameter:	DF <sub>SF6</sub>
Data unit:	Fraction
Description:	Degradation Factor of SF <sub>6</sub> that reacts with the magnesium in the production
	process assumed as 0.5
Source of data:	
Measurement	
procedures (if any):	
Any comment:	The Board after due consideration of available literature and structural design of
	the magnesium production facilities arrived at the conclusion that in absence of a
	proper system to collect the covers gases and exhaust, the uncertainties in current
	procedures to estimate the $SF_6$ destruction are very high. Therefore, a
	conservative default has been provided to ensure that emission reductions credited
	are real. Project Proponents are encouraged to submit to the DOE new procedures
	for undertaking measurement on project site to estimate the destruction efficiency.
	Procedures should be sufficiently robust, based as much as possible in
	International Standards and properly documented to ensure reliable estimates. The
	procedures should be based on experimentation of sufficient duration taking into
	account the variability in equipment used in different segments, variations in
	operating conditions/ practices, different type of alloys manufactured and similar
	other real-time production issues.

ID Number:	5
Data/Parameter:	GWP <sub>ALTGAS</sub>
Data unit:	tCO2e/ t alternative gas
Description:	Global Warming Potential of alternate gas. In case of using Perfluoro-2-methyl-3-
	pentanone the value used is 1.
Source of data:	CDM EB
Measurement	Prior to the renewal of a crediting period it should be assessed if GWP values have
procedures (if any):	changed.
Any comment:	





ID Number:	6
Data/Parameter:	DI <sub>SF6,CON,BL,k,j</sub> /DI <sub>SF6,CON,BL</sub>
Data unit:	Fraction
Description:	A conservative factor portraying the Data Integrity of $C_{SF6,CON,BL,k,j,y}/C_{SF6,CON,BL}$ in each equipment k in each segment. Default= 0.95.
Source of data:	IPCC guidelines
Measurement	Prior to the renewal of a crediting period it should be assessed if the Conservative
procedures (if any):	Factor default should be changed.
Any comment:	This value shall account for the uncertainty in SF <sub>6</sub> consumption. IPCC guidelines state that direct reporting has a 5% uncertainty level <sup>6</sup> . 0.95 shall be used as the default factor unless the project proponent can demonstrate to the DOE that their estimates of $C_{SF6,CON,BL,k,j}/C_{SF6,CON,BL}$ are more than 95% accurate. Project proponents that submit monitoring data for $C_{SF6,CON,BL,k,j}/C_{SF6,CON,BL}$ using two or more of measurement procedures listed in the monitoring section (e.g., both the weight difference and accounting method), and can consistently demonstrate a difference of less than 5% between these two estimates over the time series are allowed to multiply their SF <sub>6</sub> consumptions by a factor greater than 0.95. In no case should a factor of 100% be used.

ID Number:	7
Data/Parameter:	DI <sub>SF6,CON,PJ,k,j,y</sub>
Data unit:	%
Description:	A conservative factor portraying the Data Integrity of $C_{SF6,CON,PJ,k,j,y}$ in each segment, per year. Default= 1.05.
Source of data:	IPCC guidelines
Measurement	Prior to the renewal of a crediting period it should be assessed if the Conservative
procedures (if any):	Factor default should be changed.
Any comment:	This value shall account for the uncertainty in SF <sub>6</sub> consumption. IPCC guidelines state that direct reporting has a 5% uncertainty level <sup>7</sup> . 1.05 shall be used as the default factor unless the project proponent can demonstrate to the DOE that their estimates of $C_{SF6,CON,PJ,k,j,y}$ are more than 95% accurate. Project proponents that submit monitoring data for $C_{SF6,CON,PJ,k,j,y}$ using two or more of measurement procedures listed in the monitoring section (e.g., both the weight difference and accounting method), and can consistently demonstrate a difference of less than 5% between these two estimates over the time series should then be allowed to multiply their SF <sub>6</sub> consumptions by a factor smaller than 1.05. In no case should a factor of 100% be used.

<sup>&</sup>lt;sup>6</sup> 2006 IPCC Guidelines for NGGI pa. 4.68. <sup>7</sup> 2006 IPCC Guidelines for NGGI pa. 4.68.





ID Number:	8
Data/Parameter:	CF
Data unit:	
Description:	Conservative Factor. To compensate for the uncertainty in the global warming potential of the by products emitted after the degradation of the alternate gas (default value of 1.26 for HFC134a and 2,830 for Perfluoro-2-methyl-3-pentanone)
Source of data:	Based on the test results provided in EPA, "Characterization of Cover Gas Emissions from U.S. Magnesium Die Casting", Office of Air and Radiation, May 2004.
Measurement procedures (if any):	Prior to the renewal of a crediting period it should be assessed if the Conservative Factor should be changed, due to the publication of new experiment results or GWP values.
Any comment:	

ID Number:	9
Data/Parameter:	C <sub>SF6,TOT,BL</sub>
Data unit:	tSF <sub>6</sub>
Description:	Minimum of annual TOTAL consumption of SF <sub>6</sub> in the facility for the last three
	years prior to validation.
Source of data:	Industrial Facility
Measurement	As recommended by IPCC <sup>8</sup> , "direct reporting of $SF_6$ consumption can be
procedures (if any):	measured in the following ways:
	Recording delivered purchases and inventory changes (accounting method)
	Measuring the difference in cylinder weight for gas used/ returned (weight difference method)
	Measuring flow rates and integrating over time (flow measurement method)
Any comment:	As stated by the IPCC the first two methods are more accurate because they are
	both based on total weight used. Vintage of data should be from the last three
	years.

<sup>&</sup>lt;sup>8</sup> IPCC industrial processes 220.



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ID Number:	10
Data/Parameter:	P <sub>Mg,BL,TOTAL,y</sub>
Data unit:	tMg /yr
Description:	Amount of Mg products manufactured in baseline scenario in the facility in year y
	for each year y of the 3 years prior to the project. One year may be used if 3 years
	of data are not available (tMg/ yr).
Source of data:	Industrial Facility
Measurement	Measured by calibrated scales according to on-site working procedures
procedures (if any):	
Any comment:	Scales are usually calibrated frequently since this parameter is essential to the core
	business of the plant. Calibration frequency shall follow on-site calibration
	procedures.
	Minimum of the last three years prior to validation should be used.

# III. MONITORING METHODOLOGY

All data collected as part of monitoring should be archived electronically and be kept at least for 2 years after the end of the last crediting period. 100% of the data should be monitored if not indicated otherwise in the tables below. All measurements should be conducted with calibrated measurement equipment according to relevant industry standards.

The monitoring methodology is based on two main parameters to be monitored:

- Amount of Mg manufactured in project scenario;
- Consumption of alternate cover gas in project scenario.

In cases where SF<sub>6</sub> is used in project scenario another parameter is monitored:

• Consumption of SF<sub>6</sub> in project scenario.

In cases where CO<sub>2</sub> is used in project scenario another parameter is monitored:

• Consumption of CO<sub>2</sub> in project scenario.

Monitoring of all parameters shall be conducted separately for each segment. These parameters shall be used to calculate project emissions and dynamic ex post calculation of baseline emissions.

The industrial facility shall be in charge of supplying the data.

The parameters monitored are basic parameters that are often rigorously recorded by the industrial facility for internal purposes. The measuring instruments shall be operated and maintained by the industrial facility. Executive responsibility of carrying out periodic calibration is on the industrial facility that may conduct the calibration themselves or by an external certified company.





# Data and parameters monitored

Data / Parameter:	$P_{Mg,PJ,k,j,v}$ / $P_{MG,PJ,v}$
Data unit:	tMg/ yr
Description:	Production output: annual amount of Mg or Mg products manufactured in project scenario in each equipment $k$ in each segment $j$ per year. Annual amount of Mg
	products manufactured in project scenario in the facility per year y.
Source of data:	Industrial Facility
Measurement	Measured by calibrated scales according to on-site working procedures
procedures (if any):	
Monitoring frequency:	Continuous or per batch
QA/QC procedures:	Scale should be calibrated annually with standard weight. Figures to be cross-
	checked with internal sales and stock reports.
Any comment:	Scales are usually calibrated more than once a year since this parameter is
	essential to the core business of the plant. Calibration frequency shall follow on-
	site calibration procedures, but shall be conducted at least annually.





Data / Parameter:	Caltgas,pj,k,j,y
Data unit:	t/yr
Description:	Consumption of alternate gas in project scenario for each equipment k in each
	segment <i>j</i> per year.
Source of data:	Industrial facility
Measurement	The same procedures recommended by IPCC for direct reporting of SF <sub>6</sub>
procedures (if any):	consumption shall be practiced for the measurement of alternate gas which can be measured in the following ways:
	Recording delivered purchases and inventory changes (accounting method)
	Measuring the difference in cylinder weight for gas used/ returned (weight difference method)
	Measuring flow rates and integrating over time (flow measurement method)
	If more than one method is used for measurement, use the highest value for
	calculation of project emission.
Monitoring frequency:	Accounting Method- once purchase is made
	Weight difference method – once cylinder is replaced
	Flow measurement method - continuously
QA/QC procedures:	To ensure consistency between baseline and project calculations, the measurement method of alternate gas shall follow the same method conducted for $SF_6$ . When relying on measurements of cylinder weight or flow rates, measurements shall be cross-checked with purchase receipts. In case of uncertainty, the highest value of alternate gas shall be used resulting in the highest value for $C_{ALTGAS,PJ,k,j,y}$ and therefore the highest value of project emissions (conservative assumption). When using the weight difference method, scales should be calibrated annually using a standard weight. When using the
	flow measurement method, flow meters should be calibrated annually using an on-site standard gas sample of alternate gas or by an external certified company. The measurement of flow rate should be measured in normal cubic meter and converted to weight units. Normalization should be based on temperature and pressure readings and on the density of alternate gas.
Any comment:	As stated by the IPCC the first two methods are more accurate because they are both based on total weight used. When the accounting or weight difference method is used in casting facilities that include production of several magnesium segments (e.g. die cast & secondary magnesium) it is essential to make sure that data is recorded separately for each industry segment. If data is not recorded separately then the flow measurement method must be used.





Data / Parameter:	C <sub>SF6,CON,PJ,k,j,y</sub>	
Data unit:	tSF6 /yr	
Description:	The total consumption of SF <sub>6</sub> in the industrial facility in the project scenario in	
	each equipment in each segment, per year.	
Source of data:	Industrial facility	
Measurement	As recommended by IPCC direct reporting of SF <sub>6</sub> consumption can be measured	
procedures (if any):	in the following ways:	
	Recording delivered purchases and inventory changes (accounting method)	
	Measuring the difference in cylinder weight for gas used/ returned (weight	
	difference method)	
	Measuring flow rates and integrating over time (flow measurement method)	
	If more than one method is used for measurement, use the highest value for	
	calculation of project emission.	
Monitoring frequency:	Accounting Method- once purchase is made	
	Weight difference method – once cylinder is replaced	
	Flow measurement method - continuously	
QA/QC procedures:	To ensure consistency between baseline and project calculations, the	
	measurement method of $SF_6$ in the project scenario shall follow the same method	
	conducted for $SF_6$ in the baseline scenario. When relying on measurements of	
	cylinder weight or flow rates, measurements shall be crosschecked with purchase	
	receipts. In case of uncertainty, the highest value of $SF_6$ shall be used resulting in the highest value of project emissions (concernation). When using	
	the highest value of project emissions (conservative assumption). When using the weight difference method, scales should be calibrated annually using a	
	standard weight. When using the flow measurement method, flow meters should	
	be calibrated annually using an on-site standard gas sample of $SF_6$ or by an	
	external certified company.	
	The measurement of flow rate should be measured in normal cubic meters and	
	converted to weight units. Normalization should be based on temperature and	
	pressure readings and on the density of $SF_6$ .	
Any comment:	As stated by the IPCC the first two methods are more accurate because they are	
	both based on total weight used.	
	When the accounting or weight difference method is used in casting facilities that	
	include production of several magnesium segments (e.g. die cast & secondary	
	magnesium) it is essential to make sure that data is recorded separately for each	
	industry segment. If data is not recorded separately then the flow measurement	
	method must be used.	





Data / Parameter:	C <sub>CO2</sub> ,pJ,i,v
Data unit:	tCO <sub>2</sub> /yr
Description:	Consumption of $CO_2$ gas in project scenario for each segment <i>j</i> per year.
Source of data:	Industrial facility
Measurement procedures (if any):	The same procedures recommended by IPCC for direct reporting of $SF_6$ consumption shall be practiced for the measurement of $CO_2$ . $CO_2$ can be measured in the following ways: Recording delivered purchases and inventory changes (accounting method) Measuring the difference in cylinder/ containers weight for gas used/ returned (weight difference method) Measuring flow rates and integrating over time (flow measurement method) If more than one method is used for measurement, use the highest value for
Monitoring frequency:	calculation of project emission. Accounting Method- once purchase is made Weight difference method – once cylinder is replaced Flow measurement method - continuously
QA/QC procedures:	To ensure consistency between baseline and project calculations, the measurement method of $CO_2$ shall follow the same method conducted for $SF_6$ . When relying on measurements of cylinder weight or flow rates, measurements shall be crosschecked with purchase receipts. In case of uncertainty, the highest value of $CO_2$ shall be used resulting in the highest value of project emissions (conservative assumption). When using the weight difference method, scales should be calibrated annually using a standard weight. When using the flow measurement method, flow meters should be calibrated annually using an on-site standard gas sample of $CO_2$ or by an external certified company. The measurement of flow rate should be measured in normal cubic meter and converted to weight units. Normalization should be based on temperature and pressure readings and on the density of $CO_2$ .
Any comment:	As stated by the IPCC the first two methods are more accurate because they are both based on total weight used. $C_{CO2,PJ,y}$ is only measured when $CO_2$ is used as diluent in cover gas mix in the project activity alone (i.e. not in the baseline activity). When the accounting or weight difference method is used in casting facilities that include production of several magnesium segments (e.g. die cast & secondary magnesium) it is essential to make sure that data is recorded separately for each industry segment. If data is not recorded separately then the flow measurement method must be used.





Data / Parameter:	SO <sub>2</sub> emissions	
Data unit:	mg/m <sup>3</sup>	
Description:	SO <sub>2</sub> emissions	
Source of data:		
Measurement		
procedures (if any):		
Monitoring frequency:		
QA/QC procedures:		
Any comment:	Emissions from the facility to the ambient air should comply with the local	
	standards of the country. If no local standards exist, the following value should	
	be taken into account as a cap limit of SO <sub>2</sub> concentration in the exhausting	
	system – 1470 mg/m <sup>3</sup> (273 K, 101,325 kPa at an oxygen concentration of 6	
	%(v/v). When "dilute" SO <sub>2</sub> is the alternative gas replacing SF <sub>6</sub> and "dilute" SO <sub>2</sub>	
	emissions do not comply with the above, CERs cannot be claimed for the period	
	between the last issuance of CERs (or registration for the first verification period)	
	and the date where non-compliance was detected.	

Data / Parameter:	Magnesium sales reports	
Data unit:	tMg/ yr	
Description:	In order to dispel concerns that a company increases production levels just to gain CERs, project developers must show proof of sales of magnesium.	
Source of data:	Industrial facility	
Measurement	Annual Magnesium sales shall be compared to P <sub>Mg,PJ,iv</sub> , annual magnesium	
procedures (if any):	produced.	
Monitoring frequency:	Annually	
QA/QC procedures:	Magnesium sales reports shall be verified by DOE as part of the verification	
	process.	
Any comment:	If less than 70% of total magnesium produced is sold then the value of annual magnesium sales shall be used as the value for $P_{Mg,PJ,j,y}$ . Unless a project developer can prove to DOE that a decline in demand has occurred (due to sector price changes or other reasons) or that producing 30% more than sales is the common practice in the plant and was common practice prior to the implementation of CDM project activity.	

# IV. REFERENCES AND ANY OTHER INFORMATION

Not applicable.

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#### History of the document

Version	Date	Nature of revision(s)
02	EB 41, Annex 2	To include a changed procedure to estimate the baseline emission factor of
	02 August 2008	SF <sub>6</sub> based on the minimum value of emission factor for the three years prior to
		the start of implementation of the project activity.
01	EB 37, Annex 2	Initial adoption.
I	01 February 2008	